



Innovarpel 2025

TECHNICAL DAYS

**DIGITAL TRANSFORMATION
& INDUSTRIAL CYBERSECURITY**
IN THE OIL&GAS INDUSTRY



JUNE, 24 & 25
Rio de Janeiro, Brazil

Optimizing Inspection Strategies using Integrity-related Big Data

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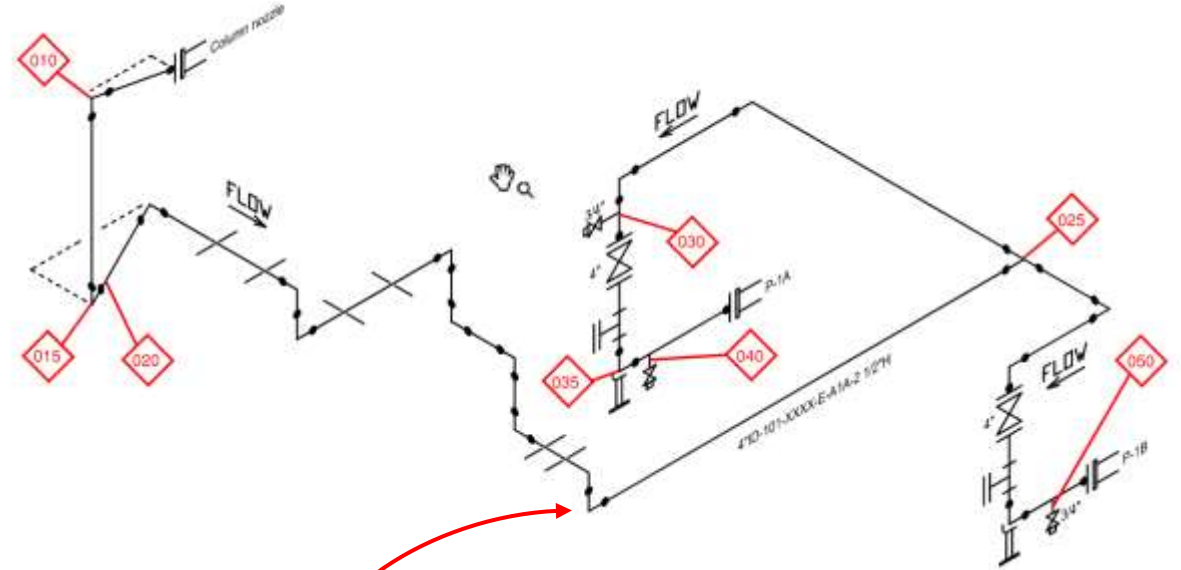


Agenda

- Disparate Integrity Data Sources
- Converting data to action (and inaction)
- Case Study Results and Benefit

Background

- **Goal:** Prevent loss of containment
- **Boundary:** Cost
- CML = Corrosion Monitoring Location
- Schedule is driven by:
 - Max time interval (per Code, such as API 570, API 510)
 - Corrosion rate and remaining life (half life inspection)
 - Optional: Risk calculation



Modern Integrity Data

CORREXPERT[®] CRUDE

Site | Unit | Resid.D06.9DP50.005

Home Export

Last Updated
6/16/25 14:00

Locations
136

Refresh Data

Live Data   

Region	Sr. No.	Location	CML #	Stream Numbe	MOC	Base Corrosion Rate	Design CR
						mpy	mpy
1	1	CDU feed transfer line		94A	9 Cr	2.4	3.1
	2	CDU feed transfer line		91A	CS	10.5	12.5
2	6	CDU feed transfer line		91D	CS	8.5	12.5
	7	CDU feed transfer line		91D	CS	9.3	12.5
	8	CDU feed transfer line		91E	CS	8.3	12.5
	9	CDU feed transfer line		91E	CS	9.0	12.5
3	10	Atm tower No. 3 stream			CS	1.4	12.5
4	11	Atm tower No. 4 stream		109A	9 Cr	1.3	3.1
5	12	Atm tower LPA		111A	9 Cr	2.1	3.1
	18	Atm tower LPA		78A	CS	4.8	12.5
	19	Atm tower LPA		113A	9 Cr	2.1	3.1
	20	Atm tower LPA		113A	9 Cr	2.1	3.1
6	21	Atm tower No. 5 stream		112A	9 Cr	6.4	3.1
	22	Atm tower No. 5 stream		112A	9 Cr	6.4	3.1
	23	Atm tower No. 5 stream		112A	9 Cr	6.4	3.1
7	24	Atm tower reduced crude		114A	9 Cr	21.4	3.1
	25	Atm tower reduced crude		114A	9 Cr	21.4	3.1
	26	Atm tower reduced crude		148A	9 Cr	21.9	3.1
	27	Atm tower reduced crude		148A	9 Cr	23.6	3.1
8	28	Atm reduced crude to Vac heater		148A	9 Cr	23.6	3.1
	29	Atm reduced crude to Vac heater		148A	9 Cr	23.6	3.1
10	33	Vac tower No. 7 stream		159A	9 Cr	3.2	3.1
	34	Vac tower No. 8 stream		79A	9 Cr	9.4	3.1
	35	Vac tower No. 8 stream		79A	9 Cr	7.1	3.1
	36	Vac tower No. 8 stream		79B	9 Cr	7.1	3.1
	37	Vac tower No. 8 stream		79B	9 Cr	7.3	3.1

Corrosion Rate

Current Target

6.5 8

CR < x < 2 * CR > 2 * CR

Alarm

Sulfur

Current Target

1.8 <1.5

< 1.8

Alert

TAN

Current Target

1.7 > 1.2

> 1.2

Alarm

Remaining Life

Current Target

11.5 10

Target

Corrosion Sensor

Current

6.3

CR < x < 2 * CR

Alert

MTD Profit

\$ 6.12M

Data Clean Up

- # Multi-factor Model

- ## Optimize Strategy

-

Case Study

- Refinery Naphtha Hydrotreater
- 74 process piping circuits (and 120 dead leg circuits)
- 1480 Historical CMLs (Avg. 5 historical readings/CML)
- All CMLs were UT locations, no historical methodology for placement
- 60% of process circuits categorized as **Tier 1**, indicating high potential for optimization

Becht Tier Summary

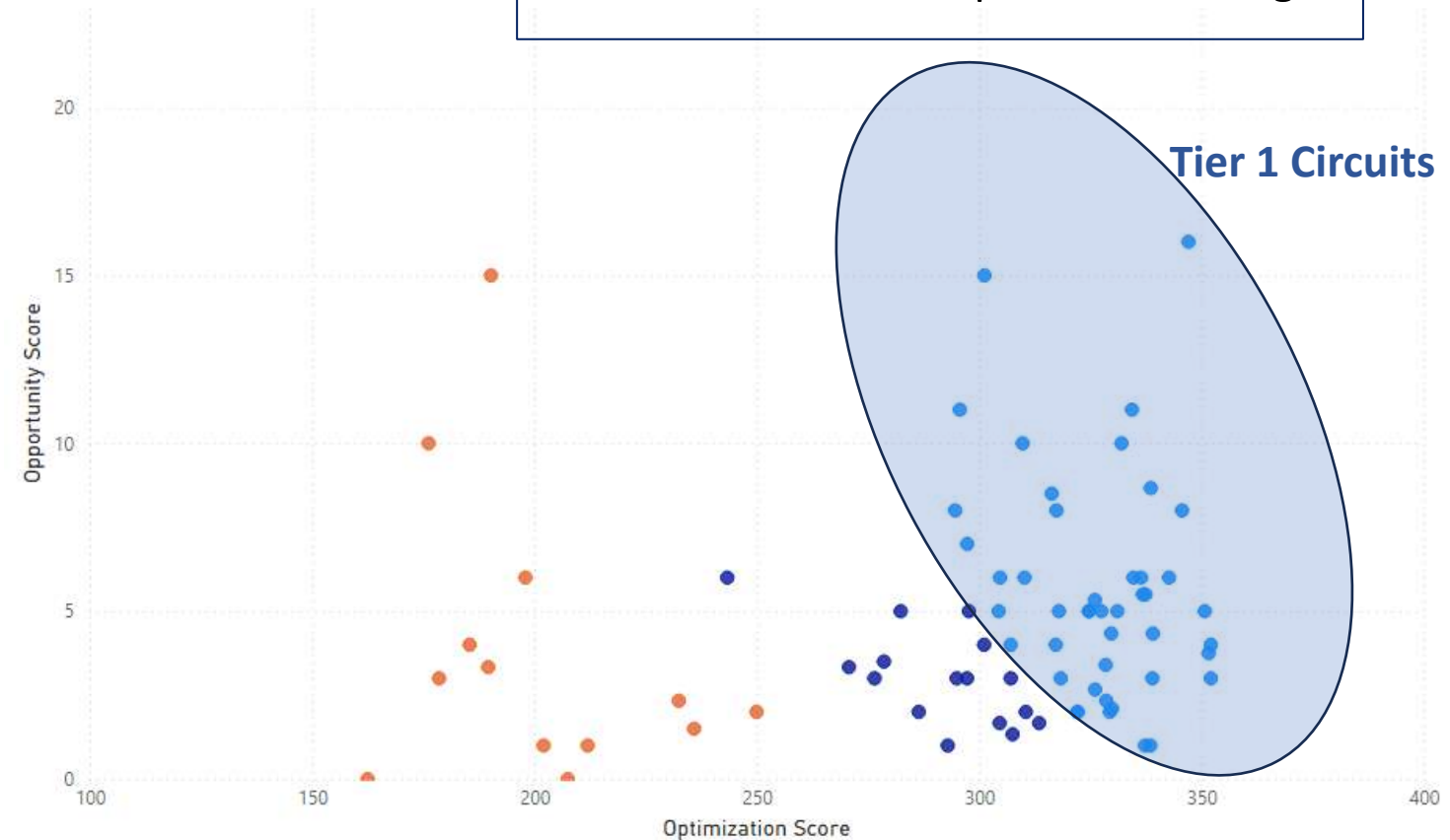
Tier 1 – Optimize, Reduce Inspection

Tier 2 – Assess, “Fine Tune” strategy

Tier 3 – Increase inspection coverage

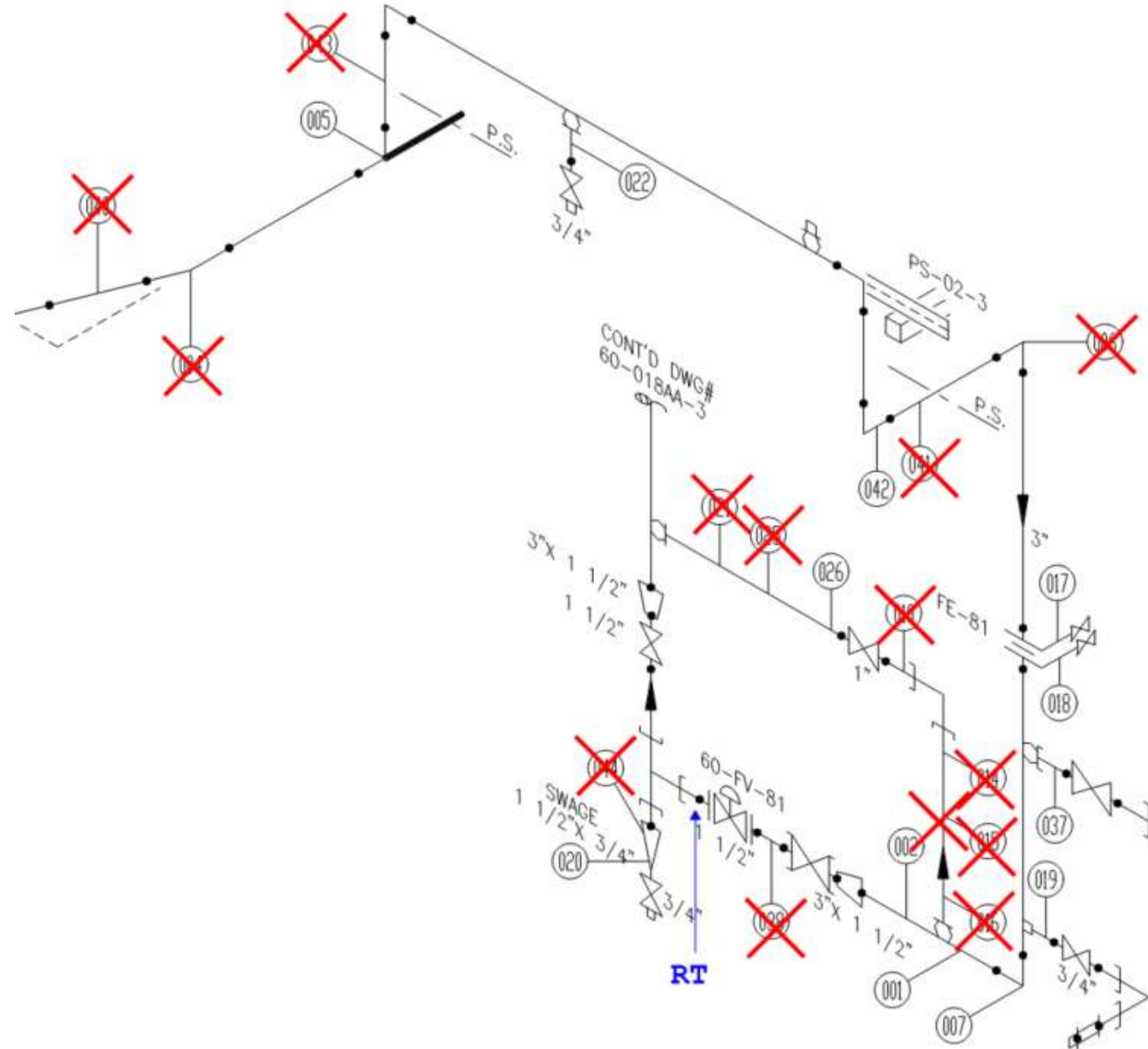
Piping Circuits by Optimization Tier

Tier ● Tier 1 ● Tier 2 ● Tier 3



Optimization Considerations

- Historical thickness data
 - Opportunity to use statistical analysis (*with restrictions*)
- Expected damage locations
 - Remove low value inspection points where damage not expected
- Expected damage rates
 - Use inspection to match expectations
 - Rely on other safeguards (like IOWs)
- NDE Methods
 - Adjust based on damage morphology



Case Study Results

- **General** Corrosion circuits - 55% CML reduction
 - Statistical tools helpful in these case
- **Localized** Corrosion circuits
 - 39% overall reduction in CML count
 - 60% of historical CMLs were modified to NDE Methods more appropriate for localized corrosion
- Significant **risk reduction** achieved through revised CML locations
- CMLs are small part of value proposition, Crude Selection Optimization (CorrExpert-Crude) adds ~\$7MM/yr savings

ORIGINAL INSPECTION COST

\$175k

48%

REDUCTION
IN CMLs

COST SAVINGS

\$75k

Plus unquantified
risk reduction

Thank you

Gracias

Obrigado

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